# JP04100807

# ANSWER 1 OF 2 CAPLUS:

ACCESSION NUMBER:

1992:491095 CAPLUS

DOCUMENT NUMBER:

117:91095

TITLE:

Thermal decomposition of polyolefins for waxes Yamanaka, Takashi; Ohori, Ryoji; Oohori, Ryoji

INVENTOR(S): PATENT ASSIGNEE(S):

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SOURCE:

Jpn. Kokai Tokkyo Koho, 7 pp.

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DOCUMENT TYPE: LANGUAGE:

Patent

FAMILY ACC. NUM. COUNT:

Japanese

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
JP 04100807	A2	19920402	JP 1990-218438	19900820
IORITY APPLN. INFO.:			JP 1990-218438	19900820

PRI Polyolefins are thermally decompd. in a tube equipped with a static mixer. AB Thus, polypropylene having limiting viscosity no. [ $\eta$ ] 1.6 dL/g was extruded and decompd. in the tube at 400° to give a polymer having  $(\eta)$  0.50 in the presence of static mixer, compared with 1.3 without the static mixer.

#### ANSWER 2 OF 2 WPIX:

ACCESSION NUMBER:

1992-162667 [20] WPIX

DOC. NO. CPI:

C1992-074872

TITLE:

Thermal decomposition wax prodn. - by feeding olefinic polymers into thermal decomposition reactor contg. static

mixing means to accelerate sepn. of formed volatile

gases.

A17

DERWENT CLASS:

PATENT ASSIGNEE(S):

(MITC) MITSUI PETROCHEM IND CO LTD

COUNTRY COUNT:

PATENT INFORMATION:

PATENT NO	KI	ND	DATE	WEEK	LA	PG
TP 04100807	Δ	1 (	9920402	(199220) *		7

### APPLICATION DETAILS:

PATENT NO	KIND	APPLICATION	DATE
JP 04100807	A	JP 1990-218438	19900820

19900820 PRIORITY APPLN. INFO: JP 1990-218438

WPIX 1992-162667 [20] AN

JP 04100807 A UPAB: 19931006

Prodn. comprises feeding olefinic polymers to a tubular thermal decomposition reactor, having an internally disposed static mixing means, to be thermally decomposed, while equalising the mixing state of a reaction mixt. passing through the tubular thermal decomposition reactor, and accelerating sepn. of volatile gases formed by thermal decomposition of the olefinic polymers from the reaction mixt. with the static mixing

#### STN Columbus

means, thereby rapidly discharging the volatile gases from the reactor.

ADVANTAGE - Thermal decomposion wax can be obtd. in high yield and efficiency which has narrow distribution of mol. wt., uniform quality and good hue.

In an example, polypropylene (intrinsic viscosity 1.6 dl/g) was thermally decomposed in a tubular thermal decomposition reactor having an internally disposed static mixer and connected with an extruder under the following conditions: extrusion rate =  $10.5 \, \text{kg/hr.}$ ; heating temp. =  $405 \, \text{deg.}$  C; internal pressure = atmospheric pressure and retention time =  $33 \, \text{min.}$ . After the volatile gases were removed from the obtd. reaction mixt. ( $400 \, \text{deg.}$  C), it was quenched to  $200 \, \text{deg.}$  C to completely stop the thermal decomposition, thereby yielding thermal decomposition wax. (0/4)